

NSF Workshop on the Emerging Applications and
Future Directions of the Boundary Element Method
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*BEM for modeling (dissipation) in
microelectromechanical systems (MEMS)*

Attilio Frangi attilio.frangi@polimi.it

Department of Structural Engineering, Politecnico di Milano

Department of Mechanics, Ecole Polytechnique, Paris



INTRODUCTION

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A. Frangi, BEM for modelling dissipation in MEMS

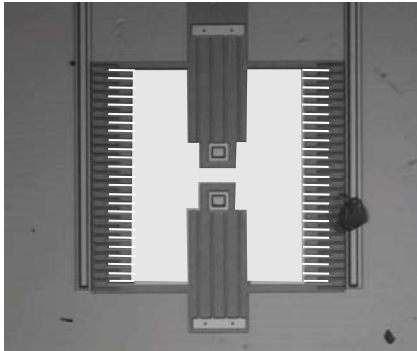
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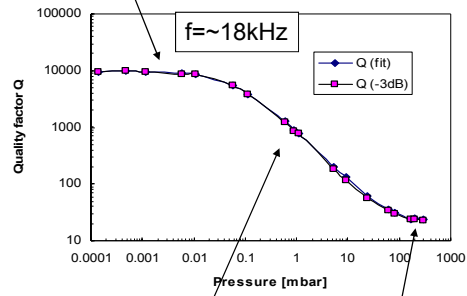
DIFFERENT SOURCES OF DISSIPATION

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Example: Tang resonator



solid/surface damping: internal friction, thermoelastic damping



fluid damping: rarefied regime

fluid damping: continuum regime

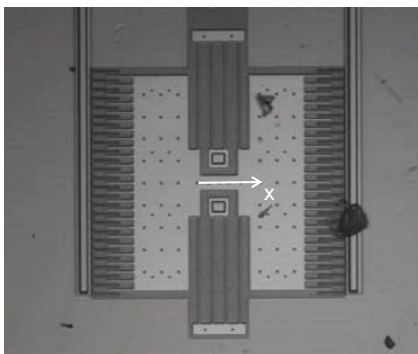
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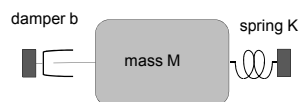
TYPICAL APPLICATION: reduced parameter model for Q extraction

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Usual assumptions:

- only springs can deform but contribution to dissipation is negligible; shuttle is *rigid* (displacement denoted by $U(t)$ w.r.t. reference to rest position)
- *small perturbations* (*linear* response)
- low resonating frequencies imply *instantaneous* fluid response



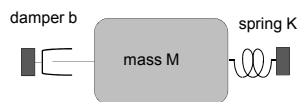
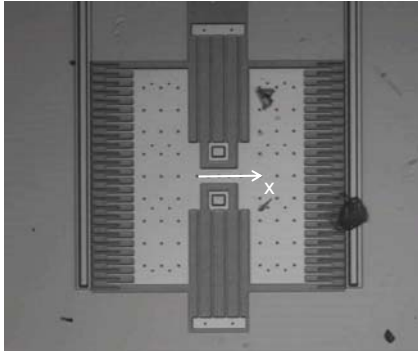
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TYPICAL APPLICATION: reduced parameter model for Q extraction

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Usual assumptions:

•only springs can deform but contribution to dissipation is negligible; shuttle is *rigid* (displacement denoted by $U(t)$ w.r.t. reference to rest position)

•small perturbations (*linear* response)

•low resonating frequencies imply *instantaneous* fluid response

As a consequence a quasi-static approach applies and the force exerted by the gas on the structure has the form:

$$\mathbf{T}(\mathbf{x}, t) = \mathbf{t}(\mathbf{x})\dot{U}(t)$$

and $\mathbf{t}(\mathbf{x})$ is a real vector function of position.

All is needed is a tool to estimate $\mathbf{t}(\mathbf{x})$ when a *unit velocity* is imposed to the shuttle

Overall gas action on structure along direction x is:

$$F(t) = \left(\int_{\partial\Omega} t_x(\mathbf{x}) dS \right) \dot{U}(t)$$

Eventually:

$$B = \int_{\partial\Omega} t_x(\mathbf{x}) dS$$

$$M\ddot{U}(t) + B\dot{U}(t) + KU(t) = F(t)$$

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REDUCED PARAMETER MODEL

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$$M\ddot{U}(t) + B\dot{U}(t) + KU(t) = F(t)$$

↓

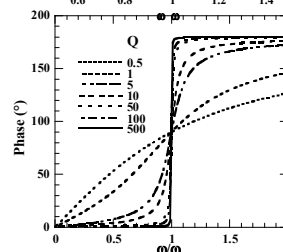
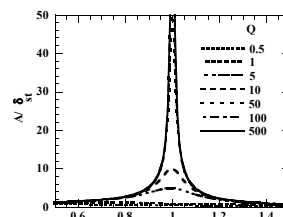
$$\ddot{U}(t) + 2\xi\omega_0\dot{U}(t) + \omega_0^2U(t) = \frac{F(t)}{M}$$

Rigorous definition of Q:

$$Q = \frac{1}{2\xi} = \omega_0 \frac{M}{B}$$

These assumptions lead to a quality factor Q which depends on pressure only through B

Q crucial in gyroscopes, magnetometers, etc...



Assumptions can be validated with phase or amplitude diagrams obtained experimentally

Impose a sinusoidal input, measure output and phase shift between input and output

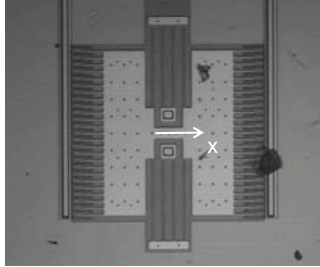
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REDUCED PARAMETER MODEL: accounting for deformability

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If also springs contribute to gas damping (and more in general when an accurate estimate of M is required accounting also for spring contribution), one typically assumes:

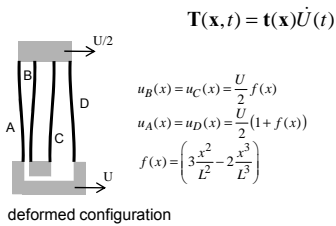
$$u(\mathbf{x}, t) = g(\mathbf{x})U(t)$$

where $g(\mathbf{x})$ is a typical mode of the structure (static or dynamic) and reduces to a constant on rigid shuttle.

Then the Principle of Virtual Power is enforced using as virtual velocity field:

$$\tilde{u}(\mathbf{x}) = g(\mathbf{x})\tilde{U}$$

$$\int_{\Omega} \tilde{u}(\mathbf{x}) \rho \ddot{u}(\mathbf{x}, t) d\Omega + \int_{\Omega} \boldsymbol{\varepsilon}[\tilde{u}(\mathbf{x})] : \boldsymbol{\sigma}[u(\mathbf{x}, t)] d\Omega - \int_{\partial\Omega} \tilde{u}(\mathbf{x}) T_x(\mathbf{x}, t) dS + \dots = 0 \quad \text{PVP}$$



$$\mathbf{T}(\mathbf{x}, t) = \mathbf{t}(\mathbf{x})\dot{U}(t)$$

If $\mathbf{t}(\mathbf{x})$ denotes the force on the structure when the velocity $g(\mathbf{x})$ is enforced, then the virtual power of viscous forces is:

$$\mathcal{P}_V(\tilde{U}, U) = \tilde{U} \left(\int_{\partial\Omega} g(\mathbf{x}) t_x(\mathbf{x}) dS \right) \dot{U}(t)$$

eventually yielding:

$$B = \int_{\partial\Omega} g(\mathbf{x}) t_x(\mathbf{x}) dS$$

$$M\ddot{U}(t) + B\dot{U}(t) + KU(t) = F(t)$$

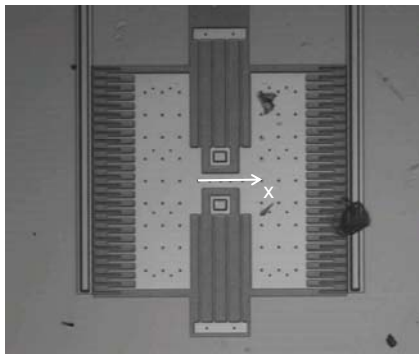
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REDUCED PARAMETER MODEL: accounting for higher frequencies

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If frequencies increase but linearity is preserved (almost always true the case of inertial MEMS), then one has to work in the frequency domain

$$u(\mathbf{x}, t) = g(\mathbf{x})Ue^{i\omega t}$$

If $\mathbf{T}(\mathbf{x}, t)$ denotes the force exerted on the structure by the fluid, then typically:

$$\mathbf{T}(\mathbf{x}, t) = \mathbf{t}(\mathbf{x}, \omega)i\omega Ue^{i\omega t}$$

with $\mathbf{t}(\mathbf{x}, \omega) \in \mathbb{C}$ hence, introducing the complex damping coefficient:

$$B(\omega) = \int_{\partial\Omega} g(\mathbf{x}) t_x(\mathbf{x}, \omega) dS$$

the final 1D model writes:

$$(-\omega^2 M + i\omega B(\omega) + K)U = F$$

with B contributing to both damping and stiffness

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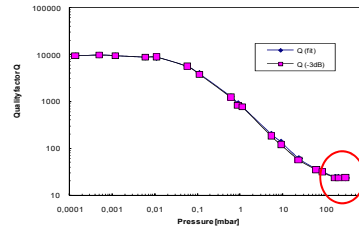
KNUDSEN NUMBER AND FLOW MODELS

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Knudsen number $Kn = \lambda/L$

λ : mean free path of molecules
 L : characteristic length scale

$\lambda = 0.069 \mu\text{m}$ at SATP, $\lambda \sim 1/p$



- Navier-Stokes equations (no-slip): $Kn \leq 10^{-3}$
- Navier-Stokes equations (slip): $10^{-3} \leq Kn \leq 10^{-1}$
- Transition regime: $10^{-1} \leq Kn \leq 10$
- Free molecular flow: $Kn > 10$

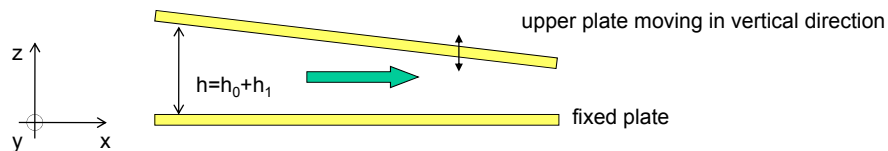
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Simplified models: linearized Reynolds equation

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typical of lubrication theory

obtained by simply imposing the mass balance equation where q_x is the total flux along x and ρ is density (indep. of z)

$$\Rightarrow \frac{\partial \rho h}{\partial t} + \frac{\partial q_x}{\partial x} = 0$$

and inserting for q_x the flux obtained from the Poiseuille parabolic velocity distribution

$$\text{then linearise w.r.t. to pressure: } p = p_0 + p_1 \Rightarrow \frac{h_0^2}{12\eta} p_0 \frac{\partial^2}{\partial x^2} \left(\frac{p_1}{p_0} \right) - \frac{\partial}{\partial t} \left(\frac{p_1}{p_0} \right) = \frac{\partial}{\partial t} \left(\frac{h_1}{h_0} \right)$$

- h_0 small w.r.t. to plate dimensions L
- variations h_1 of h_0 small w.r.t. to h_0
- isothermal process

if this term is neglected eq. is called incompressible Reynolds

various extensions to account for edge effects of rectangular and circular plates, holed plates, etc.

Blech, J. J., On Isothermal Squeeze Films, *J. Lubrication Technology*, 105, 1983.
 Bao M., Yang H., Squeeze film air damping in MEMS, *Sensors and Actuators A*, 136, 3-27, 2007 (Review)

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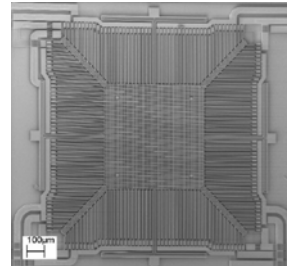
Full Navier-Stokes model and simplifications

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$$\rho \frac{\partial \mathbf{u}}{\partial t} + \rho \mathbf{u} \cdot \nabla \mathbf{u} = -\nabla p + \eta \Delta \mathbf{u} \quad \frac{\partial \rho}{\partial t} + \mathbf{u} \cdot \nabla \rho + \rho \nabla \cdot \mathbf{u} = 0$$

- ➔ **Reynolds** number $Re = UL/\nu$ (U typical speed, L typical dimension, ν kinematic viscosity)
if $Re \ll 1$ neglect non-linear convective terms in Navier Stokes
- ➔ **Mach** number $M = U/c$ (U typical speed, c speed of sound)
if $M \ll 1$ set $\nabla \cdot \mathbf{u} = 0$ (incompressibility) in Navier-Stokes
- ➔ **Stokes** number $St = fL^2/\nu$ (f vibration frequency)
if $St \ll 1$ neglect inertia terms in Navier-Stokes

Example of biaxial accelerometer (SI units):
 $L \sim 2.6 \times 10^{-6} \text{ m}$; $f = 4400 \text{ Hz}$; $\nu = 1.5 \times 10^{-5}$; $U \sim 2\pi fD$;
 $D < 1/10 L$ (D amplitude of oscillation)
 $U \sim 7 \times 10^{-3}$ $Re \sim 10^{-3}$ $M \sim 7 \times 10^{-4}$ $St \sim 7 \times 10^{-3}$



Incompressible (quasi-static) Stokes formulation

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QUASI STATIC STOKES PROBLEM

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$$\begin{aligned} \nabla p(\mathbf{x}) - \eta \Delta \mathbf{u}(\mathbf{x}) &= \mathbf{0} & \nabla \cdot \mathbf{u}(\mathbf{x}) &= 0 & \text{in } \Omega_s - \Omega \\ \mathbf{u}(\mathbf{x}) &= \mathbf{g}(\mathbf{x}) - c_t \mathbf{t}^S(\mathbf{x}) & \text{on } S \end{aligned}$$

p pressure (defined up to a constant!)
 \mathbf{u} fluid velocity, \mathbf{g} structure velocity
 $\mathbf{t} = \boldsymbol{\sigma} \cdot \mathbf{n}$ tractions, \mathbf{t}^S tractions projected on surface

$$\boldsymbol{\sigma}(\mathbf{x}) = -p(\mathbf{x})\mathbf{1} + \eta (\nabla \mathbf{u}(\mathbf{x}) + \nabla^T \mathbf{u}(\mathbf{x}))$$

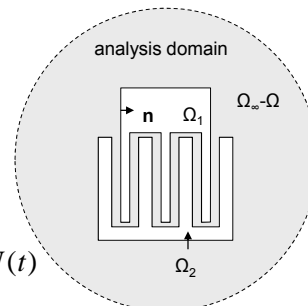
Basic assumption:
 fluid response to structure motion is instantaneous.

Time dependence?

1. inertia terms are dropped
2. velocity of structures is enforced as boundary conditions

$$\dot{\mathbf{S}}(\mathbf{x}, t) = \mathbf{g}(\mathbf{x}) \dot{U}(t)$$

STATIC STOKES PROBLEM WITH DIRICHLET BC
 formally identical to incompressible elasticity



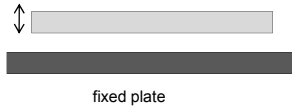
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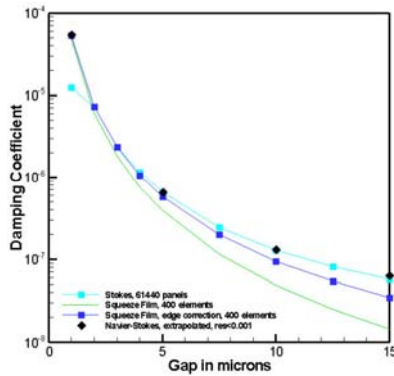


Comparison between full models and Reynolds

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Model problem to compare Navier-Stokes, Stokes, and Reynolds solutions for damping coefficients. A 50x50x4 micron plate in motion above a 60x60x4 micron plate at 1atm, 300K.



Comparison of Stokes, Reynolds Navier-Stokes, solutions

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STOKES PROBLEM BY BEM: MVT and slip BC

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$$\begin{aligned} \nabla p(\mathbf{x}) - \eta \Delta \mathbf{u}(\mathbf{x}) &= \mathbf{0} & \nabla \cdot \mathbf{u}(\mathbf{x}) &= 0 & \text{in } \Omega \\ \mathbf{u}(\mathbf{x}) &= \mathbf{g}(\mathbf{x}) - c_t \mathbf{t}^S(\mathbf{x}) & \text{on } S \end{aligned}$$

\mathbf{t} tractions, \mathbf{t}^S tractions projected on surface

$$\mathbf{t}^S(\mathbf{x}) = [\mathbf{1} - \mathbf{n}(\mathbf{x}) \otimes \mathbf{n}(\mathbf{x})] \cdot \mathbf{t}(\mathbf{x})$$

$$c_t := \frac{2 - \sigma \lambda}{\sigma \eta}$$

$$\begin{aligned} \mathbf{g}(\mathbf{x}) - \frac{c_t}{2} \mathbf{t}^S(\mathbf{x}) - \frac{\gamma}{\eta} \frac{1}{2} \mathbf{t}(\mathbf{x}) &= \int_S \left\{ \mathcal{V}(\mathbf{r}) \cdot \mathbf{t}(\mathbf{y}) + c_t [\mathcal{K}(\mathbf{r}) \cdot \mathbf{n}(\mathbf{y})] \cdot \mathbf{t}^S(\mathbf{y}) \right. \\ &\quad \left. + \frac{\gamma}{\eta} ([\mathbf{n}(\mathbf{x}) \cdot \mathcal{K}(\mathbf{r})] \cdot \mathbf{t}(\mathbf{y}) - c_t [\mathbf{n}(\mathbf{x}) \cdot \mathcal{W}(\mathbf{r}) \cdot \mathbf{n}(\mathbf{y})] \cdot \mathbf{t}^S(\mathbf{y})) \right\} dS_y \end{aligned}$$

MVT: Mixed Velocity Traction. The two equations are linearly combined



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STOKES PROBLEM BY BEM: MVT

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$$\mathbf{g}(\mathbf{x}) - \frac{c_l}{2} \mathbf{t}^S(\mathbf{x}) = \int_S \{ \mathcal{V}(\mathbf{r}) \cdot \mathbf{t}(\mathbf{y}) + c_l [\mathcal{H}(\mathbf{r}) \cdot \mathbf{n}(\mathbf{y})] \cdot \mathbf{t}^S(\mathbf{y}) \} dS_y$$

velocity equation

$$V_{ik}(\mathbf{r}) = \frac{1}{8\pi\eta} \left(\frac{\delta_{ik}}{r} + \frac{r_i r_k}{r^3} \right) \quad K_{ikq}(\mathbf{r}) = -\frac{3}{4\pi} \frac{1}{r^5} r_i r_q r_k$$

traction equation

$$\frac{1}{2} \mathbf{t}(\mathbf{x}) = \int_S \{ -[\mathbf{n}(\mathbf{x}) \cdot \mathcal{H}(\mathbf{r})] \cdot \mathbf{t}(\mathbf{y}) + c_l [\mathbf{n}(\mathbf{x}) \cdot \mathcal{W}(\mathbf{r}) \cdot \mathbf{n}(\mathbf{y})] \cdot \mathbf{t}^S(\mathbf{y}) \} dS_y$$

$$W_{qiks}(\mathbf{r}) = \frac{\eta}{4\pi} \frac{1}{r^3} \left[2\delta_{sk}\delta_{iq} + \frac{3}{r^2} (\delta_{ik}r_q r_s + \delta_{kq}r_i r_s + \delta_{is}r_k r_q + \delta_{sq}r_i r_k) - 30 \frac{r_i r_k r_q r_s}{r^4} \right]$$

very same kernels as in incompressible elasticity!!

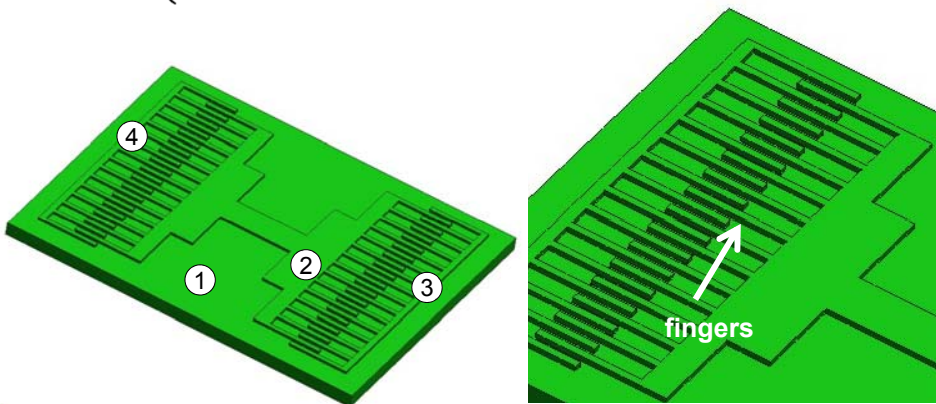


NULL SPACE OF VELOCITY EQUATION

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Exact null space vs numerical null space

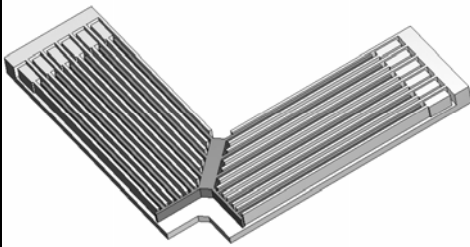
$$\mathbf{t}^\alpha(\mathbf{x}) = \begin{cases} \mathbf{n}(\mathbf{x}), & \mathbf{x} \in S^\alpha \\ 0 & \text{elsewhere} \end{cases}, \quad 1 \leq \alpha \leq N$$





WHY BEM?

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Largest problem dimension on a desktop

$$N_{\text{BEM}}: \sim \alpha 10^6$$

Equivalent FEM problem dimension

$$N_{\text{FEM}}: \sim N_{\text{BEM}}^{3/2} \sim \beta 10^9$$

Infinite extent of air domain

- No mesh of air domain
- No unknowns in air domain

Tractions are primal variables hence very good accuracy

- GMRES iterative solver
- Classical FMM with adaptive octree
- Truncation order $p \sim 8$
- Computation on the fly of near integrals
- Block diagonal preconditioning
- OpenMP parallelisation

Frangi A., Di Gioia A., Multipole BEM for the evaluation of damping forces on MEMS, *Computational Mechanics*, 37, 24-31 (2005)
 Frangi A., Tausch J., A qualocation enhanced approach for the Dirichlet problem of exterior Stokes flow, *Eng. Anal. Boundary Elem.*, 29, 86-93 (2005)
 Frangi A., Spinola G., Vigna B.: On the evaluation of damping in MEMS in the slip-flow regime, *Int. J. Num. Meth. Engng.*, 68, 1031-1051 (2006)

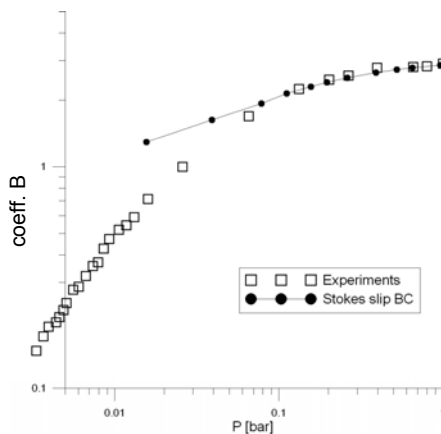
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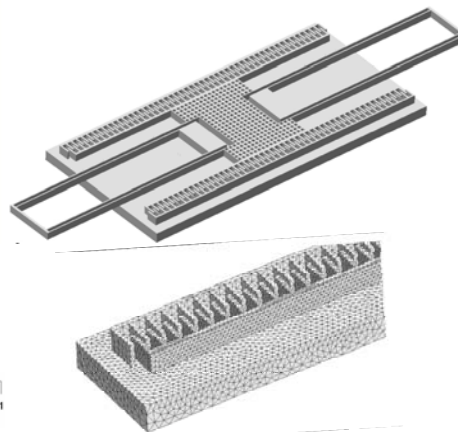


TANG RESONATOR

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diverge at low pressure
 since continuum
 model fails



$$B = \int_{\partial\Omega} t_x(\mathbf{x}) dS$$

$$M\ddot{U}(t) + B\dot{U}(t) + KU(t) = F(t)$$

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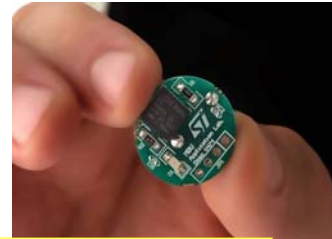
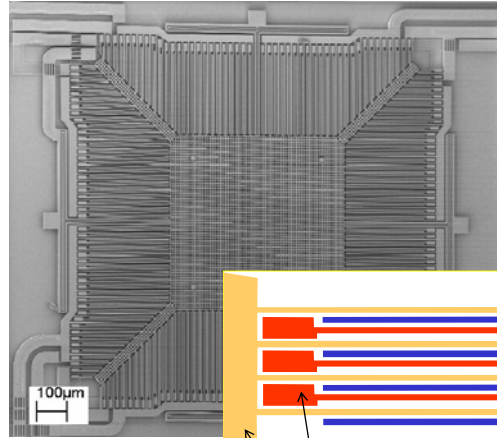
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BIAXIAL ACCELEROMETER



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$f = 4400\text{Hz}$

stator (red and orange)
Fixed to the substrate

Rotor (blue)
Mobile

Mobile mass
(holed)

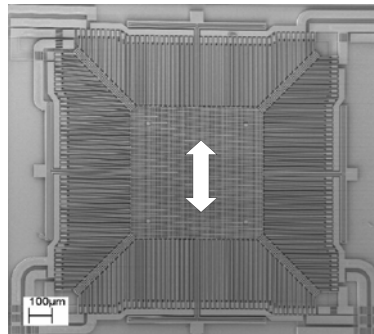
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EXPERIMENTAL VALIDATION: LINEAR ACCELEROMETER AND SLIP B.C.

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$p = 1\text{ bar}$

	Numerical "no slip"	Numerical "slip"	Experimental
Squeeze flow	$2.32 \cdot 10^{-4}\text{ N}$	$2.10 \cdot 10^{-4}\text{ N}$	-
Couette flow	$7.37 \cdot 10^{-6}\text{ N}$	$7.03 \cdot 10^{-6}\text{ N}$	-
Mass with holes	$2.10 \cdot 10^{-6}\text{ N}$	$1.94 \cdot 10^{-6}\text{ N}$	-
Total force	$2.41 \cdot 10^{-4}\text{ N}$	$2.19 \cdot 10^{-4}\text{ N}$	$2.21 \cdot 10^{-4}\text{ N}$

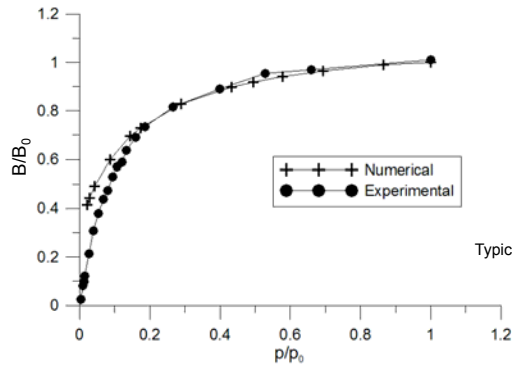
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EXPERIMENTAL VALIDATION: LINEAR ACCELEROMETER AND SLIP B.C.

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Typical comparison of simulations and results

excellent agreement at high pressure
diverge at low pressure
since continuum model fails

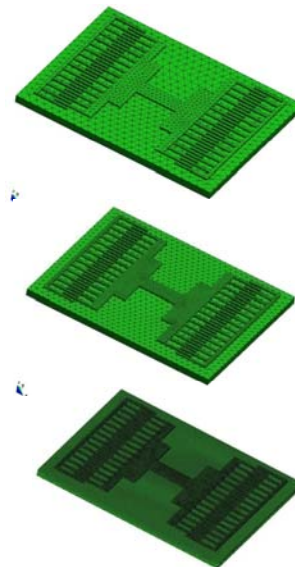
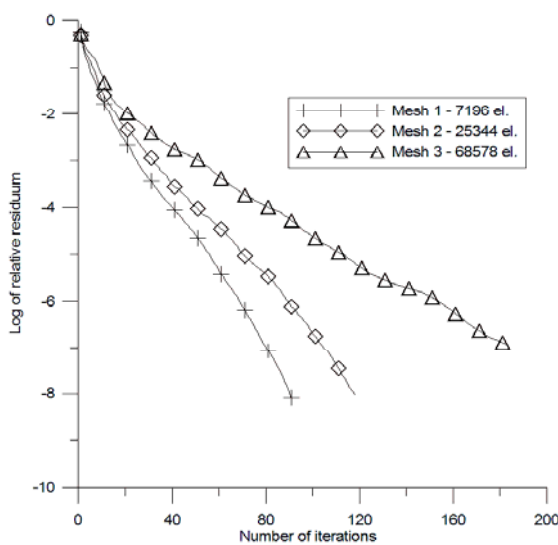
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Examples of full scale analysis: comb finger resonator

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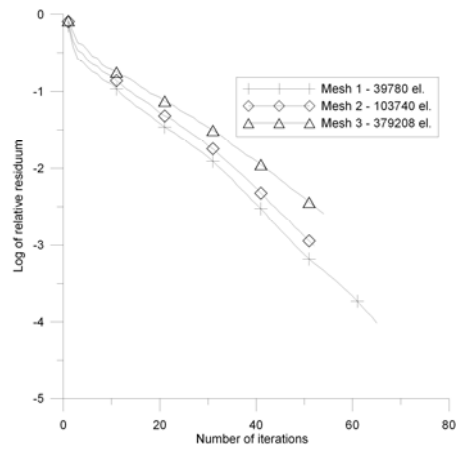
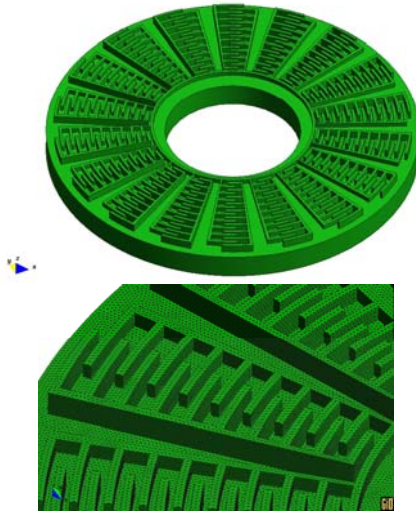
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Examples of full scale analysis: rotational resonator

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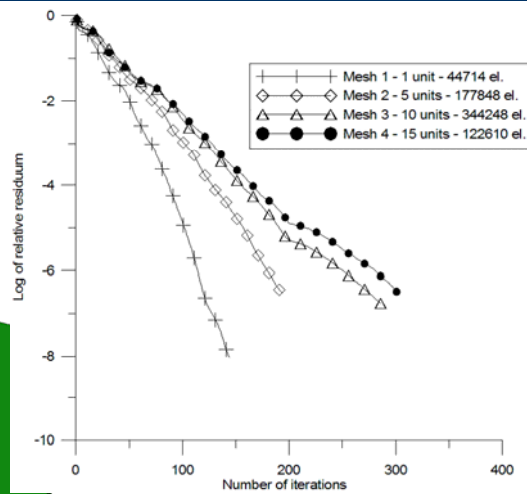
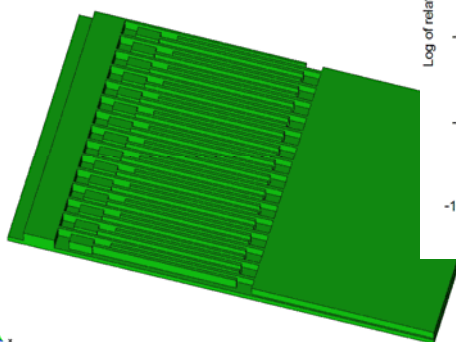
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Examples of full scale analysis: parallel plates resonator

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EXTENSION TO HIGHER WORKING FREQUENCIES

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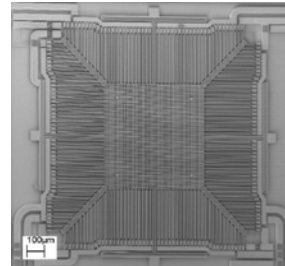
$$\rho \frac{\partial \mathbf{u}}{\partial t} + \rho \mathbf{u} \cdot \nabla \mathbf{u} = -\nabla p + \eta \Delta \mathbf{u} \quad \frac{\partial \rho}{\partial t} + \mathbf{u} \cdot \nabla \rho + \rho \nabla \cdot \mathbf{u} = 0$$

Reynolds number $Re = UL/\nu$ (U typical speed, L typical dimension, ν kinematic viscosity)
if $Re \ll 1$ neglect non-linear convective terms in Navier Stokes

Mach number $M = U/c$ (U typical speed, c speed of sound)
if $M \ll 1$ set $\nabla \cdot \mathbf{u} = 0$ (incompressibility) in Navier-Stokes

Stokes number $St = fL^2/\nu$ (f vibration frequency)
if $St \ll 1$ neglect inertia terms in Navier-Stokes

Example of biaxial accelerometer (SI units):
 $L \sim 2.6 \times 10^{-6} \text{ m}$; $f = 4400 \text{ Hz}$; $\nu = 1.5 \times 10^{-5}$; $U \sim 2\pi f D$;
 $D < 1/10 L$ (D amplitude of oscillation)
 $U \sim 7 \times 10^{-3}$ $Re \sim 10^{-3}$ $M \sim 7 \times 10^{-4}$ $St \sim 7 \times 10^{-3}$



Incompressible frequency-domain Stokes formulation



INCOMPRESSIBLE OSCILLATORY STOKES FLOW

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Mixed Velocity Traction Formulation

$$\mathbf{g}(\mathbf{x}) - \frac{\gamma}{\eta} \frac{1}{2} \mathbf{t}(\mathbf{x}) = \int_S \left\{ \mathcal{V}(\mathbf{r}) \cdot \mathbf{t}(\mathbf{y}) + \frac{\gamma}{\eta} [\mathbf{n}(\mathbf{x}) \cdot \mathcal{K}(\mathbf{r})] \cdot \mathbf{t}(\mathbf{y}) \right\} dS_y$$

$$V_{ik}(\mathbf{r}) = \frac{1}{8\pi\mu} A(R) \frac{\delta_{ik}}{r} + B(R) \frac{r_i r_k}{r^3} \quad \text{Kernels involved}$$

$$K_{iqr}(\mathbf{r}) = -\frac{\delta_{ij} r_k + \delta_{kj} r_i}{4\pi r^3} [e^{-R}(R+1) - B] - \frac{\delta_{ik} r_j (1-B)}{4\pi r^3} - \frac{r_i r_j r_k}{4\pi r^5} [5B - 2e^{-R}(R+1)]$$

$$A = 2e^{-R} \left(1 + \frac{1}{R} + \frac{1}{R^2} \right) - \frac{2}{R^2}, \quad B = -2e^{-R} \left(1 + \frac{3}{R} + \frac{3}{R^2} \right) + \frac{6}{R^2},$$

$$R = r \sqrt{\frac{-i\omega\rho}{\eta}} \Rightarrow (-1+i)r \sqrt{\frac{\omega\rho}{2\eta}}$$

if $\max(r) \sqrt{\frac{\omega\rho}{\eta}} \ll 1$ static limit recovered



$$K(\mathbf{r}) = \frac{\exp(ikr)}{4\pi r} \quad k = (\alpha + i\beta)\vartheta$$

Wave propagation in lossy media (e.g. soils). Linear constitutive relations involve complex moduli leading to complex-valued wavenumbers with $\alpha = \pm 1$ $0 < \beta < 1$ (often with $\beta \ll 1$)

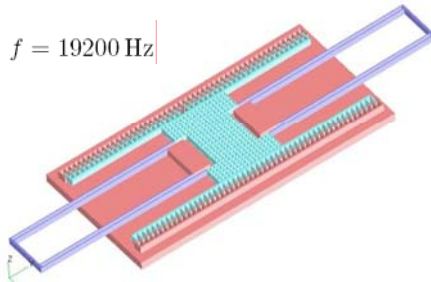
Eddy currents for the design of electrical transformers ($|\alpha| = \beta = 1$)
(Schmindlin et al. 2001)

Transient Stokes flow for the analysis of dissipation in Micro-Systems ($|\alpha| = \beta = 1$)
(Ye et al. 2003)

Computation of Casimir forces (attractive forces arising between uncharged conductive surfaces in vacuum) ($\alpha = 0, \beta = 1$)
(Reid et al. 2009)

Optical tomography with $\alpha = -1; \beta > 1$.
(Zacharopoulos et a. 2006)

Classical formulation with Gegenbauer addition theorem very effective if β is large enough w.r.t. to α
Frangi and Bonnet, CMES, 2010



Finger gap	2.88 μm
Finger length	40.05 μm
Finger overlap	19.44 μm
Center plate	54.9 \times 19.26 μm^2
Side plate1 \times 2	28.26 \times 89.6 μm^2
Side plate2 \times 4	11.3 \times 40.5 μm^2
Thickness	1.96 μm
Substrate gap	2 μm
Truss length	78 μm
Truss width	13 μm

Drag force (pN)	Steady	Unsteady
Bottom	508.75	510.72
Side	284.84	294.50
Top	102.31	142.8
Total	895.9	948.02

$$L \sqrt{\frac{\omega \rho}{\eta}} \ll 1$$



KNUDSEN NUMBER AND FLOW MODELS

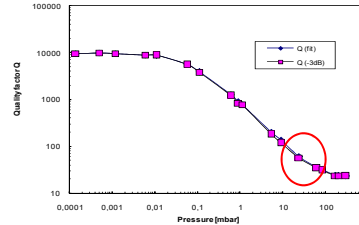
29

Knudsen number $Kn = \lambda/L$

λ : mean free path of molecules

L : characteristic length scale

$\lambda = 0.069 \mu\text{m}$ at SATP, $\lambda \sim 1/p$



- Navier-Stokes equations (no-slip): $Kn \leq 10^{-3}$
- Navier-Stokes equations (slip): $10^{-3} \leq Kn \leq 10^{-1}$
- Transition regime: $10^{-1} \leq Kn \leq 10$
- Free molecular flow: $Kn > 10$

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BGK MODEL FOR BOLTZMANN EQUATION

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$$\rho = \int_{\mathbb{R}^3} f d\xi$$

$$\rho v = \int_{\mathbb{R}^3} f \xi d\xi$$

$$T = \frac{1}{3R\rho} \int_{\mathbb{R}^3} f |\xi - v|^2 d\xi$$

$$\sigma = \int_{\mathbb{R}^3} f (\xi - v) \otimes (\xi - v) d\xi$$

$f(x, \xi)$: mass density probability depends on location x and molecular velocity ξ

mass density probability for a gas at rest

$$f_0 = \frac{\rho_0}{(2\pi RT_0)^{3/2}} \exp\left(-\frac{|\xi|^2}{2RT_0}\right)$$

rest Maxwellian

rhs accounting for molecule collisions

$$\frac{\partial f}{\partial t} + \xi \cdot \nabla f = \nu(\rho, T)(f_M - f)$$

BGK model

$$f_M = \frac{\rho}{(2\pi RT)^{3/2}} \exp\left(-\frac{|\xi - v|^2}{2RT}\right)$$

local Maxwellian

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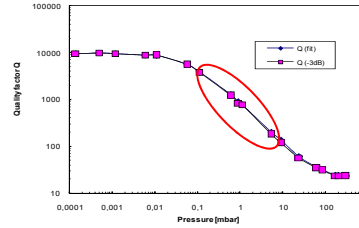
KNUDSEN NUMBER AND FLOW MODELS

31

Knudsen number $Kn = \lambda/L$

λ : mean free path of molecules
 L : characteristic length scale

$\lambda = 0.069 \mu\text{m}$ at SATP, $\lambda \sim 1/p$



- Navier-Stokes equations (no-slip): $Kn \leq 10^{-3}$
- Navier-Stokes equations (slip): $10^{-3} \leq Kn \leq 10^{-1}$
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FREE MOLECULE FLOW

$f(\mathbf{x}, \boldsymbol{\xi})$: mass density probability depends on location \mathbf{x} and molecular velocity $\boldsymbol{\xi}$

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$$\frac{\partial f}{\partial t} + \boldsymbol{\xi} \cdot \nabla f = 0$$

collisions between molecules neglected

for molecules coming from other MEMS surfaces:

$$f(\mathbf{x}, \boldsymbol{\xi}, t) = f(\mathbf{y}, \boldsymbol{\xi}, t - \frac{r}{\xi}) \quad \mathbf{y} = \mathbf{x} + \mathbf{r}, \quad \mathbf{r} = -r \frac{\boldsymbol{\xi}}{\xi}$$

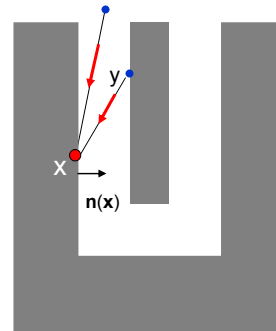
for molecules coming from far field region:

$$f(\mathbf{x}, \boldsymbol{\xi}) = f_0(\boldsymbol{\xi}) = \frac{\rho_0}{(2\pi \mathcal{R}T_0)^{3/2}} \exp\left(-\frac{|\boldsymbol{\xi}|^2}{2\mathcal{R}T_0}\right)$$

Diffuse model for molecules re-emitted from surfaces

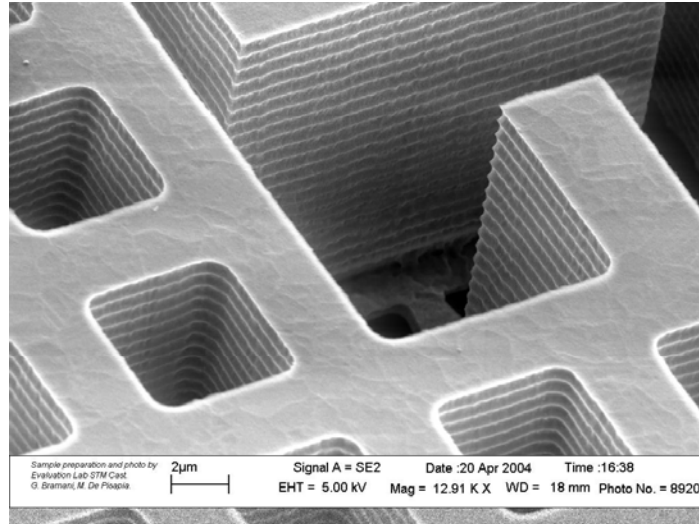
$$f(\mathbf{x}, \boldsymbol{\xi}) = \frac{\rho_w(\mathbf{x})}{(2\pi \mathcal{R}T_w(\mathbf{x}))^{3/2}} \exp\left(-\frac{|\boldsymbol{\xi} - \mathbf{w}(\mathbf{x})|^2}{2\mathcal{R}T_w(\mathbf{x})}\right) \quad \text{for } (\boldsymbol{\xi} - \mathbf{w}) \cdot \mathbf{n} > 0$$

incoming flux of molecules $\rho_w(\mathbf{x}) = \left(\frac{2\pi}{\mathcal{R}T_w(\mathbf{x})}\right)^{1/2} \int_{\mathbb{R}^3, (\boldsymbol{\xi} - \mathbf{w}) \cdot \mathbf{n} < 0} |(\boldsymbol{\xi} - \mathbf{w}) \cdot \mathbf{n}(\mathbf{x})| f(\mathbf{x}, \boldsymbol{\xi}) d\boldsymbol{\xi}$



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If shuttle velocity is small w.r.t. thermal velocity $|\tilde{w}| = |w|/\sqrt{2RT} \ll 1$.

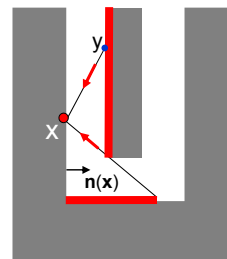
$\rho_w(\mathbf{x}, t) \simeq \rho_{w0}(1 + \rho_{w1}(\mathbf{x}, t))$ and linearise with respect to ρ_{w1} :

assuming $w(\mathbf{x}, t) = g(\mathbf{x})\dot{q}(t)$
 $\rho_{w1}(\mathbf{x}, t) = J(\mathbf{x})\dot{q}(t)$

Limit case: $\frac{\omega}{\sqrt{2RT}}L \ll 1$

$$J(\mathbf{x}) = \sqrt{\pi} \tilde{g}(\mathbf{x}) \cdot \mathbf{n}(\mathbf{x}) - \frac{1}{\pi} \int_{S^+} J(\mathbf{y}) (\mathbf{r} \cdot \mathbf{n}(\mathbf{x})) (\mathbf{r} \cdot \mathbf{n}(\mathbf{y})) \frac{1}{r^4} dS + \frac{3}{2} \frac{1}{\sqrt{\pi}} \int_{S^+} (\mathbf{r} \cdot \tilde{g}(\mathbf{y})) (\mathbf{r} \cdot \mathbf{n}(\mathbf{x})) (\mathbf{r} \cdot \mathbf{n}(\mathbf{y})) \frac{1}{r^5} dS$$

$J(\mathbf{x})$: normalised flux of molecules at the wall



Quasi static approximation: radiosity equation



Once $J(x, \omega)$ is available, compute tractions from similar BIE: $\mathcal{F}(\mathbf{p}) = t(\mathbf{x}, \omega) \mathcal{F}(i)$

$$\begin{aligned}
 -\frac{\pi^{3/2}}{\rho_0 2 \mathcal{R} T} \mathbf{t}(\mathbf{x}, \omega) &= \left(1 + \frac{1}{2} J(\mathbf{x}, \omega)\right) \frac{\pi^{3/2}}{2} \mathbf{n} + \pi \bar{g}_n(\mathbf{x}) \mathbf{n}(\mathbf{x}) + \frac{\pi}{2} \bar{\mathbf{g}}_t(\mathbf{x}) \\
 &\quad - \int_{S^+} \mathbf{r} (\mathbf{r} \cdot \mathbf{n}(\mathbf{x})) (\mathbf{r} \cdot \mathbf{n}(\mathbf{y})) \frac{1}{r^5} J(\mathbf{y}, \omega) T_4(i\bar{\omega}r) dS \\
 &\quad + 2 \int_{S^+} \mathbf{r} (\mathbf{r} \cdot \bar{\mathbf{g}}(\mathbf{y})) (\mathbf{r} \cdot \mathbf{n}(\mathbf{x})) (\mathbf{r} \cdot \mathbf{n}(\mathbf{y})) \frac{1}{r^6} T_5(i\bar{\omega}r) dS
 \end{aligned}$$

$$\begin{aligned}
 -\frac{\pi^{3/2}}{\rho_0 2 \mathcal{R} T} \mathbf{t}(\mathbf{x}) &= \left(1 + \frac{1}{2} J(\mathbf{x})\right) \frac{\pi^{3/2}}{2} \mathbf{n}(\mathbf{x}) + \pi \bar{g}_n(\mathbf{x}) \mathbf{n}(\mathbf{x}) + \frac{\pi}{2} \bar{\mathbf{g}}_t(\mathbf{x}) \\
 &\quad - \frac{3\sqrt{\pi}}{8} \int_{S^+} \mathbf{r} (\mathbf{r} \cdot \mathbf{n}(\mathbf{x})) (\mathbf{r} \cdot \mathbf{n}(\mathbf{y})) \frac{1}{r^5} J(\mathbf{y}) dS \\
 &\quad + 2 \int_{S^+} \mathbf{r} (\mathbf{r} \cdot \bar{\mathbf{g}}(\mathbf{y})) (\mathbf{r} \cdot \mathbf{n}(\mathbf{x})) (\mathbf{r} \cdot \mathbf{n}(\mathbf{y})) \frac{1}{r^6} dS
 \end{aligned}$$

static limit case

•Frangi A., Ghisi A., Coronato L., On a deterministic approach for the evaluation of gas damping in inertial MEMS in the free-molecule regime, *Sensor & Actuators, A* 149, 21–28, 2009
 •Frangi A., BEM technique for free-molecule flows in high frequency MEMS resonators, *Engineering Analysis with Boundary Elements*, 33, 493–498, 2009



TEST PARTICLE MONTE CARLO METHOD

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$\Delta \mathbf{q}$ denotes the linear momentum change of one molecule due to one collision and \mathbf{w} the instant velocity of the shuttle,

The total dissipation (energy transfer) induced by a single molecule before exiting the analysis domain through an in-flow surface is

$$d_i = \sum_c \Delta \mathbf{q} \cdot \mathbf{w}$$

for the i -th in-flow surface the number of incoming molecules per unit time is

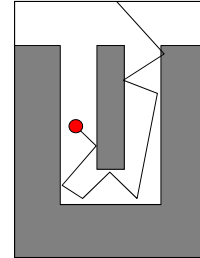
$$S_i \int_{\xi_n > 0} \xi_n f_0 d\xi = S_i \frac{\rho_0}{\sqrt{4\pi}} \sqrt{2\mathcal{R}T_0}$$

the average dissipation per unit-cycle D due to the molecules entering all the surfaces is

$$D = \frac{\rho_0 \sqrt{2\mathcal{R}T_0}}{\sqrt{4\pi}} \frac{2\pi}{\omega} \sum_i (S_i \bar{d}_i)$$

Finally the coefficient B in the 1D model is

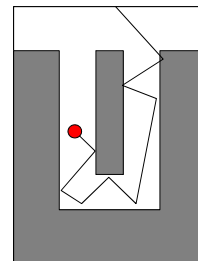
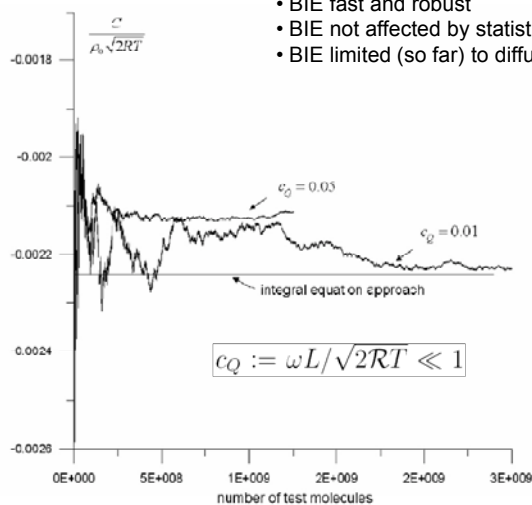
$$B = \frac{\rho_0 \sqrt{2\mathcal{R}T_0}}{\sqrt{4\pi}} \frac{2}{\omega_0^2 A^2} \sum_i (S_i \bar{d}_i)$$



BIE vs TEST PARTICLE MONTE CARLO METHOD

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- BIE independent of velocity profile imposed
- BIE fast and robust
- BIE not affected by statistical noise
- BIE limited (so far) to diffuse reflection boundary conditions



OUT-OF-PLANE ROTATIONAL RESONATOR 39

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OUT-OF-PLANE ROTATIONAL RESONATOR 40

Pressure [mbar]	Damping coefficient
0.1	0.0008
0.15	0.0012
0.2	0.0016
0.25	0.0020
0.3	0.0024
0.35	0.0028

Damping coefficient $\sim 1/Q$

Pressure [mbar]

Experimental data (black dots), Numerical (orange line)

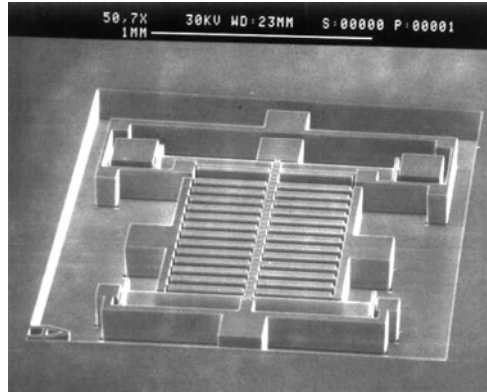
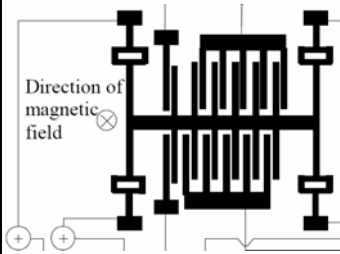
$$\rho J \ddot{\vartheta}(t) + C J \dot{\vartheta}(t) + K \vartheta(t) = M(t)$$

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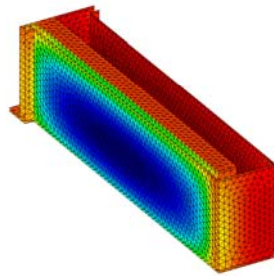


Qinetiq MAGNETOMETER

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SEM of magnetometer structure



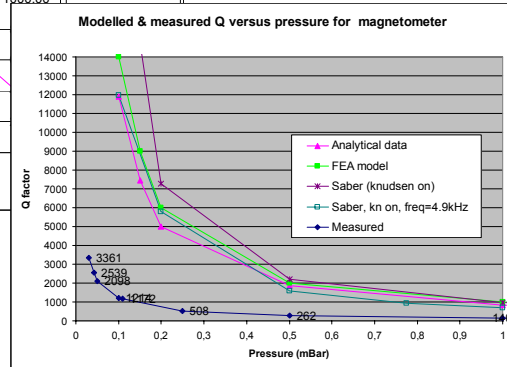
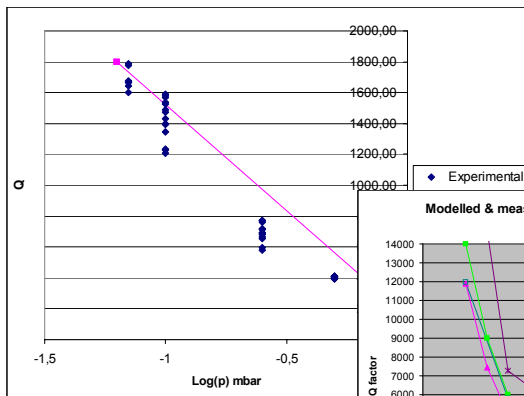
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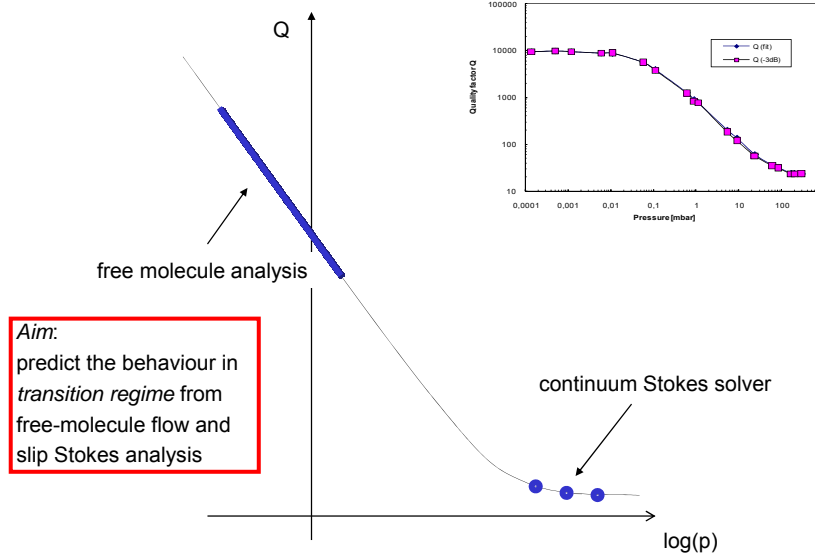
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Thank you for your attention!

